



Fig. 3 Comparison of transition data with previous literature.

It is important to emphasize that this bias occurs regardless of the magnitude of the random error. When the random error is relatively large the bias tends to be obscured. But when the random error is relatively small the bias becomes evident and emphasizes the need for care in selection of instrumentation and data reduction procedures.

Schlieren Comparison

Figure 2 is a comparison of transition times obtained from schlieren photographs with those obtained simultaneously from thin-film recordings. This figure reveals the schlieren technique to generally yield lower transition times than the thin-film recordings for the same experimental run. In this case the bias plus random error (data scatter) is a maximum of about 50%. The least square line fitting this data has a slope of 0.84 ± 0.06 with 95% confidence. Thus, the bias is about 16% in this case. The additional scatter in the data is caused by difficulty in reading or determining transition from the schlieren photographs.

Comparison with Previous Literature

Figure 3 is a comparison of the thin-film transition data from these experiments with a summary of earlier transition data presented by Hartunian, Russo, and Marrone.⁵ The cross-hatched portion of Fig. 3 shows both the range and scatter of the data presented in Ref. 5. Different symbols are used to represent the data from each shock-tube facility used in these experiments. Figure 3 shows good agreement of transition data through transition Reynolds numbers of 10^6 .

An apparent transition reversal is noted in Fig. 3 where, from shock tube No. 2, at a lower freestream temperature (smaller heat flux to the wall) the transition Reynolds numbers are extended to above values available for comparison with existing literature as well as those obtained in shock tube No. 1. This effect is well known to exist in conventional steady flow boundary layers but has only been reported in the literature⁸ for shock induced boundary layers where heat flux has been incident on the boundary layer from combustion reactions occurring in the mainstream. Some difference in transition Reynolds number from each shock tube should be expected between these facilities because of uncontrolled factors in these experiments such as freestream turbulence, surface roughness, three-dimensional effects, and shock tube size.^{3,9} Even though these differences are not quantified in these experiments the data from shock tube No. 1 compares well with the data of Ref. 5 which was obtained from a variety of facilities where, in some cases, the experimental conditions were carefully controlled. Thus, since the differences noted in Fig. 3 are larger than the possible uncertainties in the data, this reversal effect is believed to be real and is reported herein for your consideration.

References

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Minimum Length Axisymmetric Laval Nozzles

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I. Introduction

THIS paper deals with the determination of a class of minimum-length axisymmetric Laval nozzles, which are compared to the simple conical type, emphasizing the extra length needed to ensure uniform flow conditions. Submission of the paper has been prompted by the publication of Ref. 1; in fact, most of the following results have been obtained (and applied) over ten years ago, including the derivation of the hodograph equation for axisymmetric source flow, Eq. (4), but were left dormant in a journal of limited circulation.²

II. Basic Equations

Referring to Fig. 1, consider a spherical source flow, which is supersonic at distances r greater than the critical radius r_c . Writing that the mass flow m is constant at any distance:

$$4\pi r^2 \rho V = m = \text{const} \quad (1)$$

one obtains readily (see, e.g., Ref. 3, p. 372):

$$R^2 = (r/r_c)^2 = \frac{1}{M} \left(\frac{2}{\gamma+1} + M^2 \right)^{(\gamma+1)/2(\gamma-1)} \quad (2)$$

Now, along a characteristic line BB' of this source flow, the velocity vector makes an angle $\mu = \arcsin(1/M)$ with the local tangent. Therefore, one has:

$$r d\theta/dr = -\tan \mu = -1/(M^2 - 1)^{1/2} \quad (3)$$

But the ratio dr/r may be obtained by differentiating Eq. (2). After integration of Eq. (3) the following fundamental formula results:

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